

## **New Formulation for the Viscosity of Propane**

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A new viscosity formulation for propane, using the reference equation of state for its thermodynamic properties by Lemmon et al. [J. Chem. Eng. Data 54, 3141 (2009)] and valid in the fluid region from the triple-point temperature to 650 K and pressures up to 100 MPa, is presented. At the beginning, a zero-density contribution and one for the critical enhancement, each based on the experimental data, were independently generated in parts. The higher-density contributions are correlated as a function of the reciprocal reduced temperature  $\tau = T_c/T$  and of the reduced density  $\delta = \rho/\rho_c$  ( $T_c$ —critical temperature,  $\rho_c$  critical density). The final formulation includes 17 coefficients inferred by applying a state-of-the-art linear optimization algorithm. The evaluation and choice of the primary data sets are detailed due to its importance. The viscosity at low pressures  $p \le 0.2$  MPa is represented with an expanded uncertainty of 0.5% (coverage factor k=2) for temperatures  $273 \le T/K \le 625$ . The expanded uncertainty in the vapor phase at subcritical temperatures  $T \ge 273 \,\mathrm{K}$  as well as in the supercritical thermodynamic region  $T \le 423 \,\mathrm{K}$  at pressures  $p \le 30 \,\mathrm{MPa}$  is assumed to be 1.5%. In the near-critical region  $(1.001 < 1/\tau < 1.010)$  and  $0.8 < \delta < 1.2$ ), the expanded uncertainty increases with decreasing temperature up to 3.0%. It is further increased to 4.0% in regions of less reliable primary data sets and to 6.0% in ranges in which no primary data are available but the equation of state is valid. Tables of viscosity computed for the new formulation are given in an Appendix for the single-phase region, for the vapor-liquid phase boundary, and for the near-critical region. © 2016 AIP Publishing LLC for the National Institute of Standards and Technology. [http://dx.doi.org/10.1063/1.4966928]

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